



# PHY 711 Classical Mechanics and Mathematical Methods

**10-10:50 AM MWF in Olin 103**

**Notes for Lecture 29 -- Chap. 9 in F & W**

## **More hydrodynamics**

- 1. Newton's laws for fluids and the continuity equation**
- 2. Approximate solutions in the linear limit**
- 3. Linear sound waves**

	Fri, 10/18/2024	Fall Break		
24	Mon, 10/21/2024	Chap. 7	Laplace transforms and complex functions	<a href="#">#17</a>
25	Wed, 10/23/2024	Chap. 7	Complex integration	<a href="#">#18</a>
26	Fri, 10/25/2024	Chap. 8	Wave motion in 2 dimensional membranes	<a href="#">#19</a>
27	Mon, 10/28/2024	Chap. 9	Motion in 3 dimensional ideal fluids	<a href="#">#20</a>
28	Wed, 10/30/2024	Chap. 9	Motion in 3 dimensional ideal fluids	<a href="#">#21</a>
29	Fri, 11/01/2024	Chap. 9	Ideal gas fluids	<a href="#">#22</a>
30	Mon, 11/04/2024	Chap. 9	Traveling and standing waves in the linear approximation	
31	Wed, 11/06/2024	Chap. 9	Non-linear and other wave properties	

## PHY 711 -- Assignment #22

Assigned: 11/01/2024 Due: 11/04/2024

Continue reading Chapter 9 in **Fetter & Walecka**.

1. Estimate the speed of sound for the following ideal gas materials at a pressure of  $p = 101325 \text{ Pa}$  and temperature  $T = 274 \text{ K}$ :
2.  $\rho = 1.29 \text{ kg/m}^3$  (approximating dry air)
3.  $\rho = 0.18 \text{ kg/m}^3$  (approximating He gas)

Recall the basic equations of hydrodynamics

Basic variables: Density  $\rho(\mathbf{r}, t)$

Velocity  $\mathbf{v}(\mathbf{r}, t)$

Pressure  $p(\mathbf{r}, t)$

Newton-Euler equation of motion:

$$\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{v} = \mathbf{f}_{\text{applied}} - \frac{\nabla p}{\rho}$$

Continuity equation: 
$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0$$

+ relationships among the variables due to principles of thermodynamics due to the particular fluid (In fact, we will focus on an ideal gas.)

## Solution of Euler's equation for fluids -- isentropic

$$\frac{\partial \mathbf{v}}{\partial t} + \nabla \left( \frac{1}{2} v^2 \right) - \mathbf{v} \times (\nabla \times \mathbf{v}) = \mathbf{f}_{\text{applied}} - \frac{\nabla p}{\rho}$$

Additional relationships among the variables apply, depending on the fluid material and on thermodynamics

At the moment we are interested in the case where there is no heat exchange.

### A little thermodynamics

First law of thermodynamics:  $dE_{\text{int}} = dQ - dW$

For isentropic conditions:  $dQ = 0$

$$dE_{\text{int}} = -dW = -pdV \quad \begin{array}{l} \text{Here } W == \text{work} \\ \quad \quad \quad V == \text{volume} \end{array}$$

# Solution of Euler's equation for fluids – isentropic (continued)

$$dE_{\text{int}} = -dW = -pdV$$

In terms of mass density:  $\rho = \frac{M}{V}$

For fixed  $M$  and variable  $V$ :  $d\rho = -\frac{M}{V^2}dV$

$$dV = -\frac{M}{\rho^2}d\rho$$

In terms in intensive variables: Let  $E_{\text{int}} = M\varepsilon$   Internal energy per unit mass

$$dE_{\text{int}} = Md\varepsilon = -dW = -pdV = M \frac{p}{\rho^2} d\rho$$

$$d\varepsilon = \frac{p}{\rho^2} d\rho \quad \left( \frac{\partial \varepsilon}{\partial \rho} \right)_{dQ=0} = \frac{p}{\rho^2}$$

# Solution of Euler's equation for fluids – isentropic (continued)

$$\left( \frac{\partial \varepsilon}{\partial \rho} \right)_{dQ=0} = \frac{p}{\rho^2}$$

Note: Under conditions of constant entropy, we assume  $e$  can be expressed in terms of the density alone.

Consider:  $\nabla \varepsilon = \left( \frac{\partial \varepsilon}{\partial \rho} \right)_{dQ=0} \nabla \rho = \frac{p}{\rho^2} \nabla \rho$

Rearranging:  $\nabla \left( \varepsilon + \frac{p}{\rho} \right) = \frac{\nabla p}{\rho}$

Note that here we are assuming that we can write  $\varepsilon$  as  $\varepsilon(\rho, s)$ .

## Solution of Euler's equation for fluids – isentropic (continued)

$$\frac{\partial \mathbf{v}}{\partial t} + \nabla \left( \frac{1}{2} v^2 \right) - \mathbf{v} \times (\nabla \times \mathbf{v}) = \mathbf{f}_{\text{applied}} - \frac{\nabla p}{\rho}$$

$$\frac{\nabla p}{\rho} = \nabla \left( \varepsilon + \frac{p}{\rho} \right)$$

if  $\nabla \times \mathbf{v} = 0$                        $\rightarrow \mathbf{v} = -\nabla \Phi$                        $\mathbf{f}_{\text{applied}} = -\nabla U$

$$\frac{\partial(-\nabla \Phi)}{\partial t} + \nabla \left( \frac{1}{2} v^2 \right) = -\nabla U - \nabla \left( \varepsilon + \frac{p}{\rho} \right)$$

$$\Rightarrow \nabla \left( \varepsilon + \frac{p}{\rho} + U + \frac{1}{2} v^2 - \frac{\partial \Phi}{\partial t} \right) = 0$$

For isentropic and irrotational fluid.

Some details --

$$(\nabla \times \mathbf{v}) = 0 \quad \text{"irrotational flow"} \quad \Rightarrow \mathbf{v} = -\nabla\Phi$$

$$\text{Check: } (\nabla \times \mathbf{v}) = -(\nabla \times \nabla\Phi) = ?$$

$$(\nabla \times \nabla\Phi) \Big|_x = \frac{\partial^2\Phi}{\partial y\partial z} - \frac{\partial^2\Phi}{\partial z\partial x}$$

Summary: For isentropic and irrotational fluid with internal energy per unit mass  $\varepsilon$ :

$$\nabla \left( \varepsilon + \frac{p}{\rho} + U + \frac{1}{2} v^2 - \frac{\partial\Phi}{\partial t} \right) = 0$$

Here  $\varepsilon$  is the internal energy of the fluid per unit mass. For an ideal gas fluid, it has a relatively simple form.



Up to now, the assumptions on the fluid are

1. Irrotational flow
2. Isentropic (adiabatic or no heat exchange)

$$\nabla \left( \varepsilon + \frac{p}{\rho} + U + \frac{1}{2} v^2 - \frac{\partial \Phi}{\partial t} \right) = 0$$

What is  $\varepsilon(\rho, s)$ ?

Internal energy for ideal gas under isentropic conditions:

$$d\varepsilon = -\frac{p}{M} dV = \frac{p}{\rho^2} d\rho \quad (\text{from 1}^{\text{st}} \text{ "law" of thermo})$$

Internal energy for ideal gas :

$$E = \frac{1}{\gamma - 1} NkT = M\varepsilon \quad \varepsilon = \frac{1}{\gamma - 1} \frac{k}{M_0} T = \frac{1}{\gamma - 1} \frac{p}{\rho}$$

Internal energy for ideal gas under isentropic conditions:

$$d\varepsilon = -\frac{p}{M}dV = \frac{p}{\rho^2}d\rho$$

$$\left(\frac{\partial\varepsilon}{\partial\rho}\right)_s = \frac{p}{\rho^2} = \frac{\partial}{\partial\rho}\left(\frac{1}{\gamma-1}\frac{p}{\rho}\right)_s = \left(\frac{\partial p}{\partial\rho}\right)_s \frac{1}{(\gamma-1)\rho} - \frac{p}{(\gamma-1)\rho^2}$$

$$\Rightarrow \left(\frac{\partial p}{\partial\rho}\right)_s = \frac{p\gamma}{\rho}$$

For this case (adiabatic ideal gas), we can determine the relationship between  $p$  and  $\rho$ :

$$\frac{dp}{p} = \gamma \frac{d\rho}{\rho} \quad \Rightarrow d \ln p = d \ln \rho^\gamma \quad \Rightarrow p = p_0 \left(\frac{\rho}{\rho_0}\right)^\gamma$$

Some details -- Ideal gas law --  $pV = NkT = \frac{M}{M_0}kT$     $\rho = \frac{M}{V}$

Internal energy for ideal gas :

$$E = \frac{f}{2} NkT = M\varepsilon \quad \varepsilon = \frac{f}{2} \frac{k}{M_0} T = \frac{f}{2} \frac{p}{\rho}$$

In terms of specific heat ratio:  $\gamma \equiv \frac{C_p}{C_V}$

$$dE = dQ - dW$$

$$C_V = \left( \frac{dQ}{dT} \right)_V = \left( \frac{\partial E}{\partial T} \right)_V = \frac{f}{2} \frac{Mk}{M_0}$$

$$C_p = \left( \frac{dQ}{dT} \right)_p = \left( \frac{\partial E}{\partial T} \right)_p + p \left( \frac{\partial V}{\partial T} \right)_p = \frac{f}{2} \frac{Mk}{M_0} + \frac{Mk}{M_0}$$

$$\frac{C_p}{C_V} \equiv \gamma = \frac{\frac{f}{2} + 1}{\frac{f}{2}} \quad \Rightarrow \quad \frac{f}{2} = \frac{1}{\gamma - 1}$$

## Digression

Internal energy for ideal gas:  $f \equiv$  "degrees of freedom"

$$E = \frac{f}{2} NkT = M \varepsilon \quad \varepsilon = \frac{f}{2} \frac{k}{M_0} T = \frac{f}{2} \frac{p}{\rho}$$

$$\frac{f}{2} = \frac{1}{\gamma - 1} \quad \Rightarrow \quad E = \frac{1}{\gamma - 1} NkT \quad \varepsilon = \frac{1}{\gamma - 1} \frac{k}{M_0} T = \frac{1}{\gamma - 1} \frac{p}{\rho}$$

	$f$	$\gamma$
Spherical atom	3	1.66667
Diatomic molecule	5	1.40000

# Tables of specific heat ratios –

[https://www.engineeringtoolbox.com/specific-heat-capacity-gases-d\\_159.html](https://www.engineeringtoolbox.com/specific-heat-capacity-gases-d_159.html)

Gas or Vapor	Formula	Specific Heat Ratio $\kappa = c_p / c_v$
Acetone	(CH <sub>3</sub> ) <sub>2</sub> CO	1.11
Acetylene	C <sub>2</sub> H <sub>2</sub>	1.232
Air		1.40
Alcohol (ethanol)	C <sub>2</sub> H <sub>5</sub> OH	1.13
Alcohol (methanol)	CH <sub>3</sub> OH	1.26
Ammonia	NH <sub>3</sub>	1.31
Argon	Ar	1.667
Benzene	C <sub>6</sub> H <sub>6</sub>	1.12
Blast furnace gas		1.41
Bromine	Br <sub>2</sub>	1.28
Butane	C <sub>4</sub> H <sub>10</sub>	1.094
Carbon dioxide	CO <sub>2</sub>	1.289
Carbon monoxide	CO	1.40
Carbon disulphide	CS <sub>2</sub>	1.21

Back to analyzing the fluid mechanics equations

$$\nabla \left( \varepsilon + \frac{p}{\rho} + U + \frac{1}{2} v^2 - \frac{\partial \Phi}{\partial t} \right) = 0 \quad \text{For isentropic and irrotational fluid.}$$

Internal energy for ideal gas:

$$E = \frac{1}{\gamma - 1} NkT = M \varepsilon \quad \varepsilon = \frac{1}{\gamma - 1} \frac{k}{M_0} T = \frac{1}{\gamma - 1} \frac{p}{\rho}$$

$$\nabla \left( \frac{1}{\gamma - 1} \frac{p}{\rho} + \frac{p}{\rho} + U + \frac{1}{2} v^2 - \frac{\partial \Phi}{\partial t} \right) = 0$$

Also need to include continuity equation:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0$$

Now consider the fluid to be air near equilibrium

Near equilibrium:

$\rho_0$  represents the average air density

$$\rho = \rho_0 + \delta\rho$$

$p_0$  represents the average air pressure

$$p = p_0 + \delta p$$

(usually  $\approx 1$  atmosphere)

$$\mathbf{v} = \mathbf{0} + \delta\mathbf{v} = -\nabla\delta\Phi \quad \mathbf{v}_0 = \mathbf{0} \text{ average velocity}$$

$$\mathbf{f}_{\text{applied}} = \mathbf{0}$$

$$\nabla \left( \frac{1}{\gamma-1} \frac{p}{\rho} + \frac{p}{\rho} + \overset{=0}{U} + \overset{=0}{\frac{1}{2}v^2} - \frac{\partial\Phi}{\partial t} \right) = \mathbf{0}$$

$$\frac{\partial\rho}{\partial t} + \nabla \cdot (\rho\mathbf{v}) = 0$$

## Linearized equations near equilibrium

$$\left(\frac{1}{\gamma-1} + 1\right) \left(\nabla \left(\frac{p}{\rho}\right)\right) + \frac{\partial \delta \mathbf{v}}{\partial t} = 0 \quad \Rightarrow \quad \left(\frac{\gamma}{\gamma-1}\right) \left(\nabla \left(\frac{p}{\rho}\right)\right) + \frac{\partial \delta \mathbf{v}}{\partial t} = 0$$

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0$$

Further relationships for isentropic ideal gas

$$p = p_0 \left(\frac{\rho}{\rho_0}\right)^\gamma \quad \Rightarrow \quad \frac{\gamma}{\gamma-1} \nabla \left(\frac{p}{\rho}\right) = \frac{\gamma}{\gamma-1} \frac{p_0}{\rho_0^\gamma} (\gamma-1) \rho^{\gamma-2} \nabla \rho$$
$$= \frac{\gamma p_0}{\rho_0^\gamma} \rho^{\gamma-2} \nabla \rho$$

Complete linearization

$$\frac{\gamma p_0}{\rho_0^2} \nabla \delta \rho + \frac{\partial \delta \mathbf{v}}{\partial t} = 0 \quad \frac{\partial \delta \rho}{\partial t} + \rho_0 \nabla \cdot (\delta \mathbf{v}) = 0$$



Decoupling linearized equations --

$$\frac{\gamma p_0}{\rho_0^2} \nabla \delta\rho + \frac{\partial \delta \mathbf{v}}{\partial t} = 0 \quad \frac{\partial \delta\rho}{\partial t} + \rho_0 \nabla \cdot (\delta \mathbf{v}) = 0$$

$$\frac{\gamma p_0}{\rho_0} \nabla^2 \delta\rho - \frac{\partial^2 \delta\rho}{\partial t^2} = 0$$

$$\delta \mathbf{v} = -\nabla \Phi$$

$$\nabla \left( \frac{\gamma p_0}{\rho_0^2} \delta\rho - \frac{\partial \Phi}{\partial t} \right) = 0$$

$$\Rightarrow \frac{\gamma p_0}{\rho_0^2} \delta\rho - \frac{\partial \Phi}{\partial t} = \text{constant}$$

$$\Rightarrow \frac{\gamma p_0}{\rho_0^2} \frac{\partial \delta\rho}{\partial t} - \frac{\partial^2 \Phi}{\partial t^2} = 0$$

$$\frac{\gamma p_0}{\rho_0} \nabla^2 \Phi - \frac{\partial^2 \Phi}{\partial t^2} = 0$$

Have we seen these equations before?

$$\frac{\gamma P_0}{\rho_0} \nabla^2 \delta \rho - \frac{\partial^2 \delta \rho}{\partial t^2} = 0$$

$$\frac{\gamma P_0}{\rho_0} \nabla^2 \Phi - \frac{\partial^2 \Phi}{\partial t^2} = 0$$

It is also possible to show that

$$\frac{\gamma P_0}{\rho_0} \nabla^2 \delta p - \frac{\partial^2 \delta p}{\partial t^2} = 0$$

For an ideal gas under isentropic conditions with irrotational flow, close to equilibrium, the linear fluctuations in density, pressure, and velocity are characterized by a wave equation with velocity

$$c_0^2 \equiv \frac{\gamma P_0}{\rho_0}.$$

More general case -- Isentropic or adiabatic equation of state:

$$\frac{dp}{p} = \gamma \frac{d\rho}{\rho} \quad \Rightarrow \quad \frac{p}{p_0} = \left( \frac{\rho}{\rho_0} \right)^\gamma$$

Note that, next time, we will consider the more general case to find a density dependent of speed of sound for ideal gas:

$$c^2 = \left( \frac{\partial p}{\partial \rho} \right)_s = \frac{\gamma p}{\rho} \quad \text{for} \quad \frac{p}{p_0} = \left( \frac{\rho}{\rho_0} \right)^\gamma$$
$$c^2 = \frac{p_0 \gamma}{\rho_0} \frac{p / p_0}{\rho / \rho_0} = c_0^2 \left( \frac{\rho}{\rho_0} \right)^{\gamma-1} \quad \text{for} \quad c_0^2 \equiv \frac{p_0 \gamma}{\rho_0}$$

# Summary of linearized hydrodynamic equations for isentropic fluid

In terms of the velocity potential:

$$\delta \mathbf{v} = -\nabla \Phi \quad \frac{\partial^2 \Phi}{\partial t^2} - c_0^2 \nabla^2 \Phi = 0 \quad c_0^2 = \left( \frac{\partial p}{\partial \rho} \right)_{s, \rho_0}$$

In term of density fluctuation:  $\frac{\partial^2 \delta \rho}{\partial t^2} - c_0^2 \nabla^2 \delta \rho = 0$

In term of pressure fluctuation:  $\frac{\partial^2 \delta p}{\partial t^2} - c_0^2 \nabla^2 \delta p = 0$

Linearized wave equation for adiabatic ideal gas:

$$\frac{\partial^2 \Phi}{\partial t^2} - c_0^2 \nabla^2 \Phi = 0$$

$$\text{Here, } c_0^2 = \left( \frac{\partial p}{\partial \rho} \right)_s$$

$$\mathbf{v} = -\nabla \Phi$$

Note that, we also have:

$$\frac{\partial^2 \delta \rho}{\partial t^2} - c_0^2 \nabla^2 \delta \rho = 0$$

$$\frac{\partial^2 \delta p}{\partial t^2} - c_0^2 \nabla^2 \delta p = 0$$

Boundary values:

Impenetrable surface with normal  $\hat{\mathbf{n}}$  moving at velocity  $\mathbf{V}$ :

$$\hat{\mathbf{n}} \cdot \mathbf{V} = \hat{\mathbf{n}} \cdot \delta \mathbf{v} = -\hat{\mathbf{n}} \cdot \nabla \Phi$$

Free surface:

$$\delta p = 0 \quad \Rightarrow \quad \rho_0 \frac{\partial \Phi}{\partial t} = 0$$

## Boundary values of wave equation

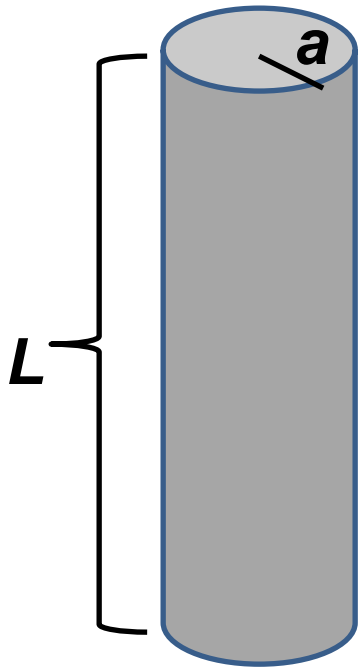
Impenetrable surface with normal  $\hat{\mathbf{n}}$  moving at velocity  $\mathbf{V}$  :

$$\hat{\mathbf{n}} \cdot \mathbf{V} = \hat{\mathbf{n}} \cdot \delta \mathbf{v} = - \hat{\mathbf{n}} \cdot \nabla \Phi$$

Free surface:

$$\delta p = 0 \quad \Rightarrow \quad \rho_0 \frac{\partial \Phi}{\partial t} = 0$$

Time harmonic standing waves in a pipe



$$\frac{\partial^2 \Phi}{\partial t^2} - c^2 \nabla^2 \Phi = 0$$

Boundary values:

At fixed surface:  $\hat{\mathbf{n}} \cdot \nabla \Phi = 0$

At free surface:  $\frac{\partial \Phi}{\partial t} = 0$